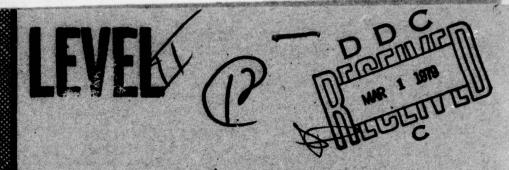


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FRANK J. SEILER RESEARCH LABORATORY

FJSRL TECHNICAL REPORT 78-0003

JUNE 1978

PARAMETERIZATION OF THE BKW AND JCZ EQUATIONS OF STATE FOR EXPLOSIVES

R. MARTIN GUIDRY RAYMOND R. MCGUIRE EDWARD L. LEE

PROJECT 2303

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AIR FORCE SYSTEMS COMMAND UNITED STATES AIR FORCE

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FJSFL-TR-78-0003

This document was prepared by the Energetic Materials Division, Directorate of Chemical Sciences, Frank J. Seiler Research Laboratory, United States Air Force Academy, Colorado. The research was conducted under Project Work Unit Number 2303-F3-04, Detonation Property Prediction and Modeling. Capt R. Martin Quidry was the Project Scientist in charge of the work.

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This report has been reviewed by the Chief Scientist and is releasable to the National Technical Information Service (NTIS). At NTIS it will be available to the general public, including foreign nations.

This technical report has been reviewed and is approved for publication.

Project Scientist

STEED WITH SAS

Directorate of Chemical Sciences

Le Colonel, USAP

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of State for Explosives	6. PERFORMING ORG. REPORT NUME
. AUTHOR(e)	8. CONTRACT OR GRANT NUMBER(s)
R. Martin/Guidry,	or sources on share nomber(s)
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FJSRL/NC	13. NUMBER OF PAGES 12
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R. Martin Guidry
Raymond R. McGuire
Edward L. Lee

TECHNICAL REPORT SRL-TR-78-0003

JUNE 1978

Approved for public release; distribution unlimited

DIRECTORATE OF CHEMICAL SCIENCES FRANK J. SEILER RESEARCH LABORATORY AIR FORCE SYSTEMS COMMAND USAF ACADEMY, COLORADO 80840

SRL-TR-78-0003

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INTRODUCTION

Computer codes for calculating realistic detonation properties are important for predicting the performance of high explosives and for assessing the usefulness of new explosive formulations. Furthermore, tremendous cost and manpower savings can be realized by the judicious use of computer codes employing an equation of state that realistically predicts detonation properties. By properly employing the computer model, the chemist can eliminate or reduce research areas showing little promise (thus saving synthesis and property evaluation costs) and concentrate on research areas offering the greatest chance of success.

The most widely used equation of state for predicting the detonation properties of condensed explosives is the semiempirical Becker-Kistiakowsky-Wilson (BKW) equation of state. This equation of state has been incorporated in thermo-hydro codes such as Fortran-BKW¹, RUBY², and TIGER³. The original equation, based on a Kistiakowsky and Wilson⁴ modification of an equation developed by Becker^{5,6,7}, has undergone many adaptions^{8,9,10}, before obtaining its current, widely used form¹¹.

$$\frac{PV}{PPT} = 1 + \chi e^{\beta \chi} \tag{1}$$

where $\chi = \kappa \sum_{i} n_{i} k_{i} / [V(T+\theta)^{\alpha}]$

In equation (1) P is the pressure of the system, V is the volume, T is the absolute temperature, and R is the ideal gas constant. The parameters α , β , κ , and θ are empirical in nature while k_i is the covolume factor



of the i^{th} detonation product species and n_i is the number of moles of the i^{th} detonation product species.

This equation was initially fit to experimental detonation data by Cowan and Fickett 11 in 1956. Later Mader 12 re-parameterized BKW to give the set of parameters $(\alpha, \beta, \kappa, \theta, k_i$'s) presently used in the Fortran-BKW code. These are shown in Tables I and II. Slightly different parameters are incorporated in the RUBY and TIGER codes.

To determine the best BKW parameters, one adjusts α , β , κ and θ and the covolume factors, k,, of the appropriate detonation product species to fit the best explosive performance data available. An estimate of the covolume factor of each species is obtainable through the hard sphere repulsion potential, r, for that species. The covolume factor and hard sphere repulsion potential are geometrically related. In the early 1960s, Mader 12 adjusted the BKW parameters to fit five experimental measurements involving two explosives, trinitrotoluene (TNT) and cyclotrimethylene trinitramine (RDX), and experimental Hugoniot data for the detonation species H2O, N2, and CO2. Using this limited data set, Mader found that two sets of parameters $(\alpha, \beta, \kappa, \theta)$ were required. (See Table I.) One set of parameters was needed for high density explosives whose detonation products contain a large amount of solid carbon (TNT-type). A second set of parameters was required for explosives whose detonation products contain a relatively small amount of solid carbon (RDX-type). Using these two parameter sets, the predictions of relative explosive performance for C.H.N.O explosives have been fairly reliable. Furthermore, absolute detonation pressures and velocities are calculated reasonably

well as long as the explosive is a C,H,N,O-type, is ideal, is near or slightly lower than CO balance and is at a high percentage of the theoretical maximum density. However, on an absolute scale the BKW predictions have not generally been accurate. Furthermore, where extremes in explosive compositions are investigated, predictions of the relative behavior are also in error. This error in relative behavior is also found when BKW predictions are made for non-C,H,N,O explosives.

The greatest deficiency of the BKW Equation of State is that it contains no attraction potential. For this reason it can be calibrated to a single point in PVT-space (as a CJ point); however, it then fits badly at all other points. Furthermore, the farther the calculated point is from the point of calibration, the worse the fit will be. Thus it is impossible to predict isentrope shapes with the BKW Equation of State.

Table I. Fortran-BWK Parameters for Explosives^a

BKW Parameter	TNT-type Value ^a	RDX-type Value
α	0.50	0.50
β	0.09585	0.16
K	12.685	10.91
θ	400.	400.

aReference 12.

Table II. Fortran-BWK Covolumes for Common Detonation Product Species

Detonation Product Species	Covolume (k _i)
н ₂ о	250
∞_2	600
α	390
N ₂	380
NO	386
H ₂	180
02	350
CH ₄	528

a Reference 12.

A second equation of state for predicting detonation properties is the Jacobs-Cowperthwaite-Zwisler (JCZ) equation of state. The equation of state, developed from first principles by Dr. Sigmund Jacobs 13, has recently been incorporated into the TIGER computer code by Cowperthwaite and Zwisler 14,15. It is anticipated that the JCZ equation of state, when properly parameterized, will offer vast improvements over the semi-empirical BKW equation of state in the calculation of not only the pressure and velocity of detonation, but also the detonation temperature, product composition and isentropic expansion from the detonation state. Unlike the BKW equation of state, the JCZ equation of state incorporates both a temperature-independent pressure term and a pressure term resulting from thermal motion. The generalized JCZ equation of state can be represented as

$$P = P_O(V, n_1 \cdots n_S) + G(T, V, n_1 \cdots n_S) NRT/V$$
 (2)

where P is the total pressure of the system, P_O is the temperature-independent pressure term, V is the volume, n_i 's are the moles of the individual product species, G is the Grüneisen parameter, R is the ideal gas constant, N is the total moles of product species, and T is the absolute temperature of the system. Furthermore, the Grüneisen parameter G is composed of several terms - one of which is a potential function. The JCZ2 equation of state incorporates the MIE potential function while the JCZ3 equation of state, the subject of this report, employs an expo-p,m potential function. In the expo-p,m potential function

$$\phi = \varepsilon \left\{ \frac{m}{p-m} \exp \left[p(1-\frac{r}{r^*}) \right] - \frac{p}{p-m} \left(\frac{r^*}{r} \right)^m \right\}$$
 (3)

or

$$\phi = \phi_{\mathbf{r}} + \phi_{\mathbf{a}} \tag{4}$$

 φ is the total potential for the pair of molecules, φ_r is the repulsion term, and φ_a is the attraction term. In equation (3) ϵ is the absolute value of the potential at its minimum, r is the molecular separation at the specified potential, r is the molecular separation at the potential minimum, p is the repulsion parameter, and m is the attraction parameter. In parameterizing the JCZ3 equation of state, one must find a best attraction parameter (m) and a best repulsion parameter (p) for the equation as a whole as well as a set of potentials (ϵ, r) for each product species encountered in the calculation. In theory it should be possible to determine these parameters from experimental Hugoniot data.

DISCUSSION

Because of the limited amount of data used, Mader's parameterization 12 of BKW was severely restricted. With an expanded data base a more severe test of the parameterization will result. Since Mader's parameterization of BKW in 1963, much useful detonation data has appeared in literature. Not only do detonation pressure and detonation velocity data for a large number of explosives abound in the literature 16,17,23, but in recent years several detonation product composition studies 18,19,20,21 have also appeared. The approach used was to select several explosives displaying a wide variety of elemental compositions on which experimental detonation pressure as a function of loading density, detonation velocity as a function of loading density, and detonation product composition data was available. The explosives selected comprised both C,H,N,O and non-C,H,N,O explosives. In Table III are listed the explosives used in this study along with their elemental compositions and experimental data available in the literature. This set of explosives should comprise a very severe test for any set of BKW parameters employed.

When the experimental detonation product composition and the BKW calculated Chapman-Jouget (CJ) isentropes are compared for both HMX and TNT, an interesting observation arises. Ornellas 18 has noted that the detonation products resulting from heavily confined charges of HMX and TNT attain equilibrium under nonideal gas conditions between approximately 1500°K and 1800°K. The RUBY code was used to calculate the CJ isentropes at these two temperatures for HMX and TNT. The experimental product composition should then fall within the range of values for the

Explosives Used in the Reparameterization of the BKW Equation of State Along With Experimental Detonation Properties Table IIIa.

Name	Composition	Formula	Density (g/cc)	Detonation Pressure (kilobars)	Detonation Velocity (m/sec)
HPCK	Cyclotetramethylene tetranitramine	C4H8N8O8	1.90 1.89	390	9110
THE STATE OF THE S	2,4,6-Trinitrotoluene	c ₇ H ₅ N ₃ O ₆	1.64	210	6940
BIF	Benzotrifuroxan	C _N 60	1.86	360	8480
FX-23AA	Hydrazine Nitrate/ Hydrazine-78.4/21.6	H6.96 ^N 3.81 ^O 2.47	1.42	280	8640
RX-23AB	Hydrazine/H ₂ 0 - 69.05/5.1/25.9	H7.28 ^N 2.49 ^O 3.61	1.38	190	7790
RK-23AC	Hydrazine Nitrate/ Hydrazine-32.4/67.6	H _{10.15} N _{5.21} O _{1.05}	1.15	175	1960
BTNEA	Bis-trinitroethyl adipate	C ₁₀ H ₁₂ N ₆ O ₁₆	1.59	215	7200

Reference 23

Explosives Used in the Reparameterization of the BKW Equation of State Along With Experimental Detonation Product Compositions Table IIIb.

			Mole	Moles Product/Kilogram Explosive	t/Kilog	ram Expl	osive		
Name	Composition	N ₂	н20	ω_2 ω NH ₃ H ₂ CH ₄	8	NH ₃	Н2		(s)
нж	Cyclotetramethylene tetranitramine	12.43ª,b	10.74 6.48	6.48	3.56	3.56 1.33 1.01 0.13	1.01	0.13	3.28
TML	2,4,6-Trinitrotoluene	5.81 ^a	7.04 5.50	5.50	8.72	8.72 0.71 2.03 0.44	2.03	0.44	16.07
BIF	Benzotrifuroxan	11.62 ^b		6.19	11.38	1	•	ı	6.23
RK-23AA	Hydrazine Nitrate/ Hydrazine-78.4/21.6	16.42 ^b	25.73 ^d	1.	•	4.91	1.20	•	1
RK-23AB	Hydrazine Nitrate/ Hydrazine/H.O- 69.05/5.1/25.9	12.70 ^b	35.51	1		0.18	0.07	1	1
RK-23AC	Hydrazine Nitrate/ Hydrazine-32.4/67.6	13.10 ^b	13.10 ^e		•	23.00 1.90	1.90	1	
BINEA	Bis-trinitroethyl adipate	5.72 ^C	9.00 8.62	8.62	7.58	7.58 0.78 1.55	1.55	0.28	4.57

Reference 18

Preference 19

Reference 21

diffeoretical maximum is 24.74 moles H₂0 per kilogram RX-23AA

Theoretical maximum is 10.50 moles H2O per kilogram RX-23AC

1500°K and 1800°K calculated isentropes since in this range the product species composition is "frozen". The comparison can be seen in Table IV for HMX and TNT. In both cases it is immediately obvious that the calculated quantity of CO is much smaller than the observed quantity while the calculated amount of CO $_2$ is much larger than the observed amount of this product species. Furthermore, the observed amount of C $_{(s)}$ falls very near the lower end of the calculated range for this product species.

The relative quantities of these three carbon-containing species are governed by equilibrium

$$2\infty_{(g)} \xrightarrow{} \infty_{2(g)} + C_{(s)}$$
 (5)

Mader assumed formation of carbon in the standard state (i.e., $\Delta H_f = 0$); however, it may be noted that the above equilibrium can be shifted to the left by increasing the heat of formation of $C_{(s)}$ — which is input into the computer. The BKW calculated isentropes would then contain more CO and less CO_2 and $C_{(s)}$. This is in the correct direction to satisfy the deficiencies discussed above. It was thus decided to add an additional parameter— the heat of formation of $C_{(s)}$ — in the reparameterization of the BKW equation of state. Added impetus to this decision was the observation that the carbon produced was not graphite but an amphorous form. Additionally, several other researchers (particularly scientists at Lawrence Livermore Laboratory and in the Soviet Union) were using positive heats of formation for carbon in their computer codes.

There are very few measurements of detonation temperatures at the CJ state and these have relatively large uncertainties 12,22. Nevertheless, it was intuitively felt that the calculated detonation temperatures should

be higher. For a fixed set of the other BKW parameters, $(\alpha, \beta, \kappa, \kappa_i's)$, the larger the value of the parameter θ , the higher the calculated detonation temperature.

The approach taken, therefore, in reparameterizing the BKW equation of state was the systematic variation of the five empirical parameters $(\alpha,~\beta,~\kappa,~\theta~and~\Delta H_{\mbox{\scriptsize f}}^{\mbox{\scriptsize C}})$ while providing for the dependence of detonation temperature on θ and the dependence of equation (5) on the heat of formation of C(s). Additionally, each product species has a characteristic covolume, k. These product species' covolumes were also treated as empirical parameters; however, they were constrained within certain, reasonable limits and not allowed to completely vary. In the parameterization, not only were detonation pressures and velocities used in the fit, but also product composition. Furthermore, the fit was extended to include the non-C,H,N,O explosives BTF, RX-23AA, RX-23AB and RX-23AC as well as the C,H,N,O explosives HMX, TNT and BINEA. These extensions should give a very severe test of the BKW equation of state both from the standpoint of the wide range of explosive properties used in the parameterization as well as the types of explosives employed in the fit attempt.

The results of this "brute force" parameterization attempt are given in Tables V and VI. The "best" fit set of parameters and product specie colvolumes are displayed in Table VII. The results shown in Tables V and VI are exceptionally good considering the wide range of detonation properties fit and the various types of explosives used. Comparison of calculated results with experimental data demonstrates that the differences between the two are usually within the known experimental error which is

TABLE IV. Comparison of the BKW Calculated CJ Isentrope Products with the Observed Products from Heavily Confined Charges of HMX and TNT

		p'q'MH			p'qIMI		
PRODUCT SPECIES	OBSERVED	BKW CJ ISENTAOPE 1520°K	BK CJ ISENTROPE 1800°K	OBSERVED	BKW CJ ISENTROPE 1505°K	BKW CJ ISENTROPE 1835°K	
(s) ₂	3.28	3.82	5.67	16.07	15.71	19.81	8 8
8	3.56	0.34	0.24	8.72	2.47	1.41	
82	6.48	8.07	7.19	5.50	9.64	8.41	
п20	10.74	10.50	12.39	7.04	4.67	8.23	
N_2	12.43	13.40	13.40	5.81	95.9	6.52	
H ₂	1.01	0.02	0.00	2.03	0.19	0.07	
E 3	1.33	0.26	0.25	0.71	0.11	0.21	
₽	0.13	1.28	0.37	0.44	2.99	1.19	

Reference 18.

bunits of moles of product species per kilogram of explosive.

Density of 1.89 grams per cc.

density of 1.53 grams per ∞ .

Comparison of the Reparameterized BKW Calculated CJ Isentrope Products with the Observed Products from Heavily Confined Charges of Various Explosives Table V.

State of Solved	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	HWA,b,c			TMTA, b	
Product Species	Observed	1515°K Isentrope	1776°K Isentrope	Observed	1476°K Isentrope	1775°K Isentrope
C _(S)	3.28	2.87	4.08	16.07	14.91	18.03
8	3.56	3.56	2.94	8.72	8.75	86.9
82	6.48	19.9	6.42	5.50	2.87	2.60
Н20	10.74	10.12	11.23	7.04	5.93	8.23
N ₂	12.43	12.97	13.02	5.81	6.33	6.28
2	1.01	0.97	0.69	2.03	1.68	1.36
M ₃	1.33	1.06	0.97	11.0	0.55	99.0
G,	0.13	0.41	90.0	0.44	1.29	0.21

Table V. Continued.

Product Species	Observed	BINEA ^{a,d} 1519°K Isentrope	1816°K Isentrope	Observed	RX-23AA ^{a,C} 1483°K Isentrope	1783°K Isentrope
(s)	4.57	3.36	5.58			1000
8	7.58	8.53	7.32			
82	8.62	8.42	8.14			
п20	9.00	8.51	10.29	25.73 ^e	24.72	24.72
N ₂ .	5.72	9.09	6.04	16.42	16.37	16.16
Н2	1.55	1.54	1.19	1.20	2.02	1.38
MA.	0.78	0.62	0.63	4.91	5.40	5.82
₽	0.28	0.87	0.14			

Table V. Continued

		RX-23ABa,c			RK-23ACa,c	
Product Species	Observed	1484°K Isentrope	1769°K Isentrope	Observed	1493°K Isentrope	1831°K Isentrope
Н,0	35.51	36.11	36.11	13.10 [£]	10.50	10.50
' K'	12.70	12.37	12.37	13.10	13.53	13.06
E E	0.18	0.16	0.17	23.00	25.04	25.98
.	0.07	90.0	0.04	1.90	2.69	1.28
						76,73
	松	BIFA,C			BIT.A,C	
Product Species	Observed	1527°K Isentrope	1846°K Isentrope	Observed	2163°K Isentrope	2564°K Isentrope
(s)	6.23	5.07	4.79	6.23	5.67	6.65
8	11.38	14.21	13.66	11.38	12.45	10.49
	6.19	5.07	4.79	6.19	2.67	99.9
N ₂	11.62	11.90	11.90	11.62	11.90	11.90
^a Units of Moles Product Species per Kilogram Explosive ^b Reference 18 ^c Reference 19 15	oduct Species	per Kilogram I	Aplosive	dreference 21 Crimeoretical H20 per Ki H20 per Ki	Reference 21 Theoretical Maximum is 24.74 Moles H2O per Kilogram RX-234A Theoretical Maximum is 10.50 Moles H2O per Kilogram RX-23AC	74 Moles A .50 Moles

Comparison of the Reparameterized BKW Calculated CJ Detonation Properties With the Observed Detonation Properties of Heavily Confined Charges of Various Explosives Table VI.

Explosive (Density- gm/cc)	Detonation Pressure (kiloatm) Calc Exp	tion re m) Exp ^a	Detonation Velocity (Meters/sec) Calc Exp	rion :y :/sec) Exp	Detonation Temperature (°K) Calc Exp	
HWK (1.90)	401	390	9415	9110	3082	Details.
INT (1.64)	661	210	7116	6940	2693 –	
BINEA (1.59)	228	215	7580	7200	3031 –	
EX-23AA (1.420)	244	280	8268	8640	2324 2900	
FX-23AB (1.379)	178	190	7532	7790	1769 4000	
RK-23AC (1.153)	172	175	7995	1960	1904 2180	
BFT (1.86)	343	•	8429	8480	4258 –	

Reference 23

Table VII. "Best" Fit Reparameterized BKW Parameters and Covolumes

Parameter	Reparameterize BKW Value	đ		
α	0.50			
β	0.176			
K	11.80			
θ .	1850			
AH ^C	12.0			
Covolumes	-			
0	440			
ω_2	610			
н ₂ о	270			
N ₂	404			
н ₂	98	,		
NH ₃	384		1	
CH ₄	550			
NO	386			18 TA
02	325			

generally no better than 5%. Again in accordance with Ornellas' findings (18), a "freeze-out" temperature range of 1500°K-1800°K has been employed for calculated detonation product composition data.

Because the JCZ3 equation is developed from first principles and, therefore, the parameters do have physical significance, it was felt that a purely "brute force" type of fit would be unsatisfactory. The values assigned to the parameters should be determined from experimental data and, therefore, should be physically meaningful. Fortunately, for many of the detonation product species, experimental Hugoniot data does exist. For each of these product species then, the pair potential parameters (ε/k, r*) can be determined. First, however, the attraction and repulsion parameters (m,p) of the JCZ equation of state must be set. Because this equation of state was ideally written for spherical molecules in a face-centered cubic (fcc) lattice structure, it is necessary to find experimental Hugoniot data for a spherical molecule with a face-centered cubic lattice structure that can be used to set the value of the attraction and repulsion parameters as well as its own pair potential parameters. A molecule for which much experimental data is available and which satisfies the above requirements is argon (24-28). Once the attraction and repulsion parameters are determined from argon Hugoniot data, they are used unchanged in the determination of the pair potential parameters for each of the detonation product species. Because the product species are not generally of a spherical shape and often do not pack in a face-centered cubic lattice structure, small deviations from the "true" pair potential values are expected. The detonation product species for which experimental

Hugoniot data are available are water (H_2O) (29), nitrogen (N_2) (30,31), carbon dioxide (CO_2) (30), oxygen (O_2) (32), and hydrogen (H_2) (28, 33-35).

The procedure used in establishing the values of the attraction and repulsion parameters and the pair potential parameters was to use the TIGER computer code to calculate a Hugoniot curve for the species of interest. This curve was compared with the experimental Hugoniot curve. Adjustments were made to the parameters until the fit was within experimental error. By working with Hugoniot data in setting the parameter values as opposed to actual detonation property data of explosives, one restricts the number of variables that must be simultaneously adjusted to obtain a reasonable fit. With the exception of argon, only two variables must be adjusted to obtain the pair potential parameters for any one species. If detonation property data were employed, one would be required to simultaneously adjust all of the pair potential parameters of the product species as well as the attraction and repulsion parameters. This would be a very laborious task. Furthermore, it is very likely that the "best" fit pair potential parameters could no longer be related to physical properties of the system since there would be a tendency to spread deviations over all parameters. It is essential, therefore, that care be taken to insure realistic values for the pair potential parameters. Estimates of these parameters, based on physical measurements, can be obtained from several sources (13,36,37). It should be remembered that the calculated parameters will vary slightly from the measured values because of the restrictions of the JCZ3 equation of state. Once the pair potential parameters of species for which experimental Hugoniot data exist have been determined,

then these parameters for the other product species (CH₄, NH₃, NO, CO) must be evaluated. This can be accomplished by obtaining initial estimates (13,36,37) of the parameters and then using detonation product data from several explosives. As new product species are added to the TIGER library, it will be necessary to determine the pair potential parameters.

In order to facilitate the parameterization of the JCZ3 equation of state, a subroutine was incorporated into the TIGER computer program. This subroutine, based on the method of Bevington (38), simultaneously varies either two (ϵ/k , r*, p), three (ϵ/k , r*, p), or four parameters (ϵ/k , r*, p, m) until a "best" fit set of parameters are obtained. The "best" fit parameters are ascertained by a comparison of the experimental Hugoniot data, which is input, and the calculated Hugoniot data. A "quality of fit" parameter was used to determine when a satisfactory fit of the Hugoniot data is obtained. For all species except argon only the two-parameter option was employed. With argon, both the three- and the four-parameter options were used in an attempt to obtain a satisfactory fit. When the three-parameter option was employed, the value of the attraction parameter was set equal to 6.0 for which there appears to be some theoretical justification (36).

This attempt to parameterize the JC23 equation of state has demonstrated two major problem areas. In the analysis of argon attempts to vary all four parameters (ε/k , r^* , p, m) met with no success - primarily because the temperature of the system reached extremely high values during the calculations causing the program to terminate with an error. This is strictly a software problem - not a theoretical one. When the attraction

parameter was set at 6.0 and the other three parameters for argon were varied, a minimum chi square value was obtained. At this minimum the repulsion parameter was 14.330, ϵ/k was 48.98 and r* was 3.93. However, when the attraction parameter was set at 6.0, the value of the repulsion parameter was readjusted for each run and only two parameters were simultaneously varied, no overall minimum could be located. These results are shown in Table VIII. The value of the chi square appears to vary inversely with the value of the repulsion parameter. At values of the repulsion parameter above 14.5, the calculated temperatures become extremly high and the program terminates by error. Furthermore, the values of the pair potential parameters become very unrealistic for high values of "p". No explanation is forthcoming about why the two points at "p" equal to 14.33 are not equivalent. It is most certainly due to a peculiarity in the fitting subroutine. The second problem area concerns the fit of the calculated Hugoniot curve to the experimental Hugoniot curve. The data shown in Table IX is typical of that obtained on all fit attempts. The calculated and experimental Hugoniot curves typically fit very well at the high pressure segment of the curve; however, at the lower pressures (below 30 kiloatmospheres) the fit becomes increasingly unsatisfactory. This result demonstrates the need to reexamine the JCZ3 equation of state particularly at the low pressure end where most of the detonation products are in the gas phase or between the gas and normal liquid state. Because no values of the attraction and repulsion parameters could be obtained, the parameterization attempt is suspended until the reevaluation of the JCZ3 equation of state is accomplished.

Table VIII. Attempted Fit for Liquid Argon Hugoniot Using Simultaneous Variation of ϵ/k and r^* With m=6.0 and Various Input Values of p.

ε/	k	r*	Chi	Square	
45	0.0	3.34		26.51	
31	5.1	3.43		21.28	10000
21	0.3	3.53		17.91	
13	6.5	3.65		15.73	
12	5.0	3.67	Chica Chica	15.41	
11	4.1	3.70		15.10	
9	4.2	3.75		14.57	
8	6.4	3.77		14.33	
6	3.2	3.87		13.70	
5	3.5	3.91		13.43	

a Reference 26.

Table IX. Typical Fit Attempt of Calculated and Experimental Hugoniot Curves for Liquid Argon (ϵ/k = 48.98, r* = 3.93, p = 14.33, m = 6.00)

Input Volume (cc/gm)	Exp. Pressure (atmos.)	Calc. Pressue (atmos)	% Error
0.5585	6713.	12253.	45.2
0.5259	11727.	16535.	29.1
0.5026	17965.	21141.	15.0
0.4851	25426.	25955.	2.0
0.4780	30000.	28385.	-5.7
0.4600	40000.	36189.	-10.5
0.4460	50000.	44545.	-12.2
0.4316	59421.	56210.	-5.7
0.4184	74064.	71090.	-4.2
0.4071	90248.	88163.	-2.4
0.3975	107973.	107400.	-0.5
0.3892	127237.	128681.	1.1
0.3819	148042.	151793.	2.5
0.3754	170386.	176426.	3.4
0.3697	194272.	202156.	3.9
0.3646	219697.	228480.	3.8
0.3600	246663.	254819.	3.2
0.3558	275169.	280618.	1.9
0.3520	305215.	305429.	0.0
0.3486	336801.	328938.	-2.4
0.3454	369928.	351005.	-5.4

a Reference 26.

CONCLUSION

The BKW equation of state has been successfully reparameterized. The reparameterized version of this equation of state is far superior to any previous versions in that it not only satisfactorily predicts detonation pressures and detonation velocities for ideal (C,H,N,O) explosives, but also predicts these properties as well as detonation product compositions for both ideal and non-ideal explosives. The two major changes in the reparameterization were a significant increase in the value of the parameter θ and the addition of a fifth parameter - the heat of formation of amorphous carbon. In considering the data in Table V, one notes that BTF is the only explosive where significant deviations from the experimental data are calculated. It is believed that for BTF the "freeze out" temperature range may be significantly higher than the 1500°-1800°K range employed. BTF appears to be a much hotter-burning explosive than any of the other explosives used. As shown in Table V, when a 2150°-2550°K "freeze-out" range is used, the fit is very good. Another point should be noted regarding this reparameterized BKW equation of state. After the reparameterization was completed, an error in one of the methane thermodynamic constants (15) was discovered. The thermodynamic constants for all product species are given in Appendix A. As long as the reparameterized BKW equation of state is used with this incorrect value, the results should be satisfactory. The new parameters compensate for the error in the incorrect methane thermodynamic constant. If this error is corrected, a new parameterization must be accomplished.

Attempts to parameterize the JC23 equation of state were unsuccessful. It is felt that the primary reason for this is that the equation itself needs to be revised in order to better calculate detonation properties at lower pressures. Once the equation has been revised, attempts at parameterization of the equation can continue. Once satisfactorily parameterized, the JC23 equation of state should be far superior to any other equation of state currently being used.

APPENDIX A

Thermodynamic Constants for Gaseous Detonation Product Species in the Reparameterized BKW Equation of State

Product Species	ਰ	8	ខ	2	ઇ	૪	D	8	ච
N ₂	5.75413	-0.33702	0.04832	0.04832 -0.00237 -2.22510	-2.22510	0.79188	0.79188 -0.09545	-4520.2	52.9446
н20	5.70892	1.12992	-0.23397	0.01670	0.01670 -2.57395	1.07622	1.07622 -0.14489 -61903.4	-61903.4	51.4737
82	9.19922	0.45824	0.07053	0.07053 -0.00334 -2.86534	-2.86534	0.06480	-0.06049	0.06480 -0.06049 -102713.0 61.1172	61.1172
8	5.83223	-0.40052	0.06451	0.06451 -0.00371 -2.13408	-2.13408	0.71371	0.71371 -0.08177 -31127.4	-31127.4	54.5275
4	2.83501	0.90236	-0.14779	-0.14779 0.01011 -0.13223	-0.13223	0.21837	0.21837 -0.04345	-1105.1	39.0572
GH,	18.15476	1.09409	0.10650	0.10650 -0.00355 -11.79180	-11.79180	3.70291	-0.41517	3.70291 -0.41517 -36874.0	34.3221 ^a
MH ₃	8.19429	1.46088	-0.28032	-0.28032 0.02233 -3.66338	-3.66338	1.13155	-0.12635	1.13155 -0.12635 -18629.4	51.7146
20	4.07999	0.26535	0.00277	-0.00280	0.00277 -0.00280 -0.00439	-0.20149	0.04394	-3303.1	56.2805
2	5.72913	0.39180	0.06717	0.06717 -0.00411 -1.79711	-1.79711	0.53528	0.53528 -0.05361	16865.8	57.9890

a Incorrect value. Corrected value is 41.2172

APPENDIX B

Thermodynamic Constants for Solid Detonation Product Species in the Reparameterized BKW Equation of State

Product Species	ਰ	8	ខ	25	ស	8	Б	8	ව
(s) ₂	4.175	4.175 -0.4439 -0.08374	-0.08374	-0.004587	-1.802	-1.802 -0.07144	-0.01429 7070.0 ^a	7070.0ª	3.731

1.191E-09 -6.378E-06 1.192E-10 -3.756E-15 3.583E-12 -1010E-16 0. 0. 0.	· A	2 A1	A ₁₃ A ₂₁	A22	A ₃₁	A32	A33 A41 A42 A43	A41 A42	A43
			1E-09 -6.378E	-06 1.192E-10	-3.756E-15	3.583E-12	-1010E-16	0. 0.	

 $^{\text{A}}_{\text{C8}} = (\Delta H_{\text{f}}^{\text{C}} - 4930.0) \text{ calories mole}^{-1}$

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